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# Nanostructured electrode enabling fast and fully-reversible $\text{MnO}_2$ -to- $\text{Mn}^{2+}$ conversion in mild buffered aqueous electrolytes

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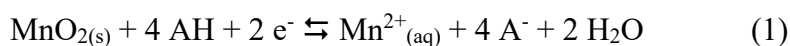
## Abstract

On account of their low-cost, earth abundance, eco-sustainability, and high theoretical charge storage capacity, MnO<sub>2</sub> cathodes have attracted a renewed interest in the development of rechargeable aqueous batteries. However, they currently suffer from limited gravimetric capacities when operating under the preferred mild aqueous conditions, which leads to lower performance as compared to similar devices operating in strongly acidic or basic conditions. Here, we demonstrate how to overcome this limitation by combining a well-defined 3D nanostructured conductive electrode, which ensures an efficient reversible MnO<sub>2</sub>-to-Mn<sup>2+</sup> conversion reaction, with a mild acid buffered electrolyte (pH 5). A reversible gravimetric capacity of 560 mA·h·g<sup>-1</sup> (close to the maximal theoretical capacity of 574 mA·h·g<sup>-1</sup> estimated from the MnO<sub>2</sub> average oxidation state of 3.86) was obtained over rates ranging from 1 to 10 A·g<sup>-1</sup>. The rate capability was also remarkable, demonstrating a capacity retention of 435 mA·h·g<sup>-1</sup> at a rate of 110 A·g<sup>-1</sup>. These good performances have been attributed to optimal regulation of the mass transport and electronic transfer between the three process actors, *i.e.* the 3D conductive scaffold, the MnO<sub>2</sub> active material filling it, and the soluble species involved in the reversible conversion reaction. Additionally, the high reversibility and cycling stability of this conversion reaction is demonstrated over 900 cycles with a Coulombic efficiency > 99.4 % at a rate of 44 A·g<sup>-1</sup>. A Zn/MnO<sub>2</sub> cell configuration is also demonstrated, and we discuss the key parameters governing the efficiency of the MnO<sub>2</sub>-to-Mn<sup>2+</sup> conversion. Overall, the present study provides a comprehensive framework for the rational design and optimization of MnO<sub>2</sub> cathodes involved in rechargeable mild aqueous batteries.

## Introduction

The development of rechargeable aqueous batteries for large-scale electrochemical energy storage devices is driven by their ability to achieve appropriate energy densities with safe, sustainable and inexpensive chemicals.<sup>1,2</sup> Among the different aqueous batteries, the rechargeable Zn/MnO<sub>2</sub> battery, able to operate in a mild aqueous electrolyte, is certainly the most attractive, especially since the breakthrough of Pan et al. in 2016,<sup>3</sup> who demonstrated a high reversibility and excellent cycling stability when using a mild acidic electrolyte containing both ZnSO<sub>4</sub> and MnSO<sub>4</sub>. Since then, the concept has been declined in many studies, varying the nature of the MnO<sub>2</sub> cathode and the chemical composition of the Zn<sup>2+</sup>-based aqueous electrolyte.<sup>4</sup> Despite all these efforts, however, the gravimetric capacities of mild aqueous Zn/MnO<sub>2</sub> batteries remain capped to 350-380 mA·h·g<sup>-1</sup>,<sup>4-6</sup> which is far from the maximal theoretical value of 617 mA·h·g<sup>-1</sup> associated with the reversible 2-electron reduction of Mn(IV) into Mn(II).

Recently, we have revealed that the charge storage mechanism at MnO<sub>2</sub> electrodes is not based on an insertion process but instead on a reversible conversion principle, wherein the weak Brønsted acid AH and conjugated base A<sup>-</sup> present in an aqueous buffered electrolyte assist the following proton-coupled electron transfer reaction at the electrode interface:<sup>7</sup>



According to this reaction, the 2-electron gravimetric capacity of MnO<sub>2</sub> should be accessible in mild, non-corrosive buffered aqueous media, which according to the Pourbaix diagram lies within the domain of thermodynamic stability of Mn<sup>2+</sup>.<sup>8</sup> In our previous work, the maximal gravimetric capacity achieved in a buffered electrolyte of pH 5 was 450 mA·h·g<sup>-1</sup> (obtained from MnO<sub>2</sub> thin films electrodeposited onto planar electrodes).<sup>7</sup> Although much better than those capacities previously reported for a range of MnO<sub>2</sub>-cathodes in mild unbuffered aqueous electrolytes, this gravimetric capacity remains far from the 570 mA·h·g<sup>-1</sup> value recently achieved in a strongly

acidic electrolyte (*i.e.*, 0.1 M H<sub>2</sub>SO<sub>4</sub>).<sup>9</sup> In this case, a similar conversion reaction is at work, but with H<sub>3</sub>O<sup>+</sup>/H<sub>2</sub>O acting as the proton donor/acceptor couple. Further studies are thus required to better understand the key factors and parameters currently limiting the MnO<sub>2</sub>-to-Mn<sup>2+</sup> conversion in mild aqueous electrolytes. Our previous work leads us to believe that two issues are critical: (*i*) the efficiency of the electrical wiring between the MnO<sub>2</sub> solid phase and the underlying current collector, and (*ii*) the appropriate regulation of both the electron transport/transfer at the electrode/MnO<sub>2</sub> film/electrolyte interface and the mass transport of all soluble species involved in reaction 1 (*i.e.*, Mn<sup>2+</sup>, AH, and A<sup>-</sup>).<sup>10</sup> Indeed, if misbalanced, the Coulombic efficiency (*CE*) lies below 100 %, inducing a progressive decrease of the electrode gravimetric capacity upon cycling because of the incomplete exploitation of MnO<sub>2</sub>.<sup>7</sup>

Concerning the electron transfer between the semi-conductive MnO<sub>2</sub> and the current collector, a few studies have reported on the poor adhesion and mechanical stability of MnO<sub>2</sub> on conductive substrates of various chemical composition and roughness.<sup>11,12</sup> Furthermore, because of the moderate electronic conductivity (10<sup>-3</sup>-10<sup>-4</sup> S·cm<sup>-1</sup>) of MnO<sub>2</sub>, the ohmic drop is expected to rise together with the film thickness. All these issues can potentially be solved by using a 3D nanostructured current collector with a high aspect ratio, well-suited for the conformal electrodeposition of thin films of MnO<sub>2</sub> to provide shorter ion diffusion distances and better electron harvesting paths.<sup>10,13</sup> Such a strategy has previously been successfully exploited to improve the performances of MnO<sub>2</sub>-based supercapacitors,<sup>14-16</sup> as well as MnO<sub>2</sub> cathodes toward reversible Li<sup>+</sup> insertion in organic electrolytes.<sup>17</sup>

To achieve good conformal electrodeposition of MnO<sub>2</sub> over a 3D porous conductive substrate, the latter must necessarily have a well-opened structure with accessible porosity to avoid any mass transport limitation of the soluble species involved in reaction 1. The technique also requires

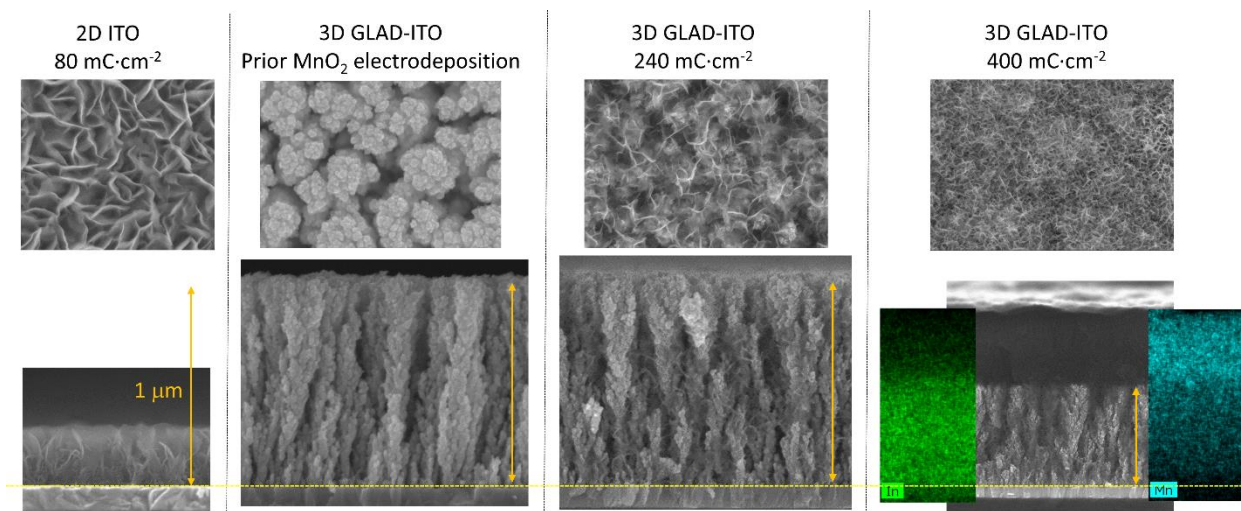
proper matching of the reactant concentrations and the conversion fluxes, which are linked to both the cycling rate and the specific area developed by the 3D conductive scaffold. In addition, due to the stoichiometry of the conversion process (4 equivalents of proton donor required, see eq 1), strong pH gradients may be generated at the electrode/electrolyte interface, inducing the concomitant precipitation of insoluble phases such as zinc hydroxide sulfates (ZHS), as evidenced in several studies.<sup>3,18–22</sup> We believe this point contributes to the limited gravimetric capacities previously observed with unbuffered mild aqueous Zn/MnO<sub>2</sub> batteries.<sup>23</sup> To solve this issue, one strategy is to regulate the pH at the metal oxide/electrolyte interface, using a mild acidic buffered electrolyte at a sufficiently high concentration.<sup>7</sup>

In the present study, we demonstrate the decisive advantage of using a nanostructured current collector to fully exploit the reversible MnO<sub>2</sub>-to-Mn<sup>2+</sup> conversion from a buffered aqueous electrolyte containing Mn<sup>2+</sup>. We also show that this conversion reaction remains highly efficient even in a Zn/MnO<sub>2</sub> battery cell configuration, which involves a Zn foil anode paired to the MnO<sub>2</sub> cathode and the presence of Zn<sup>2+</sup> ions, in addition to Mn<sup>2+</sup>, in the buffered electrolyte. For such purpose, we took advantage of 3D nanostructured indium-doped tin oxide (ITO) electrodes (1- $\mu$ m-thick film deposited over a standard flat ITO-coated glass substrate) prepared by glancing angle deposition (GLAD), a technique which allows for the growth of metal oxide nanostructures in different shapes and morphologies.<sup>24</sup> These model mesoporous electrodes are characterized by a reproducible morphology with high aspect ratio and opened porosity,<sup>25</sup> well-suited for modification by electrodeposition as previously shown with conductive polymers.<sup>26</sup> In addition, their transparency allows for *in-situ* UV-vis spectroelectrochemical monitoring, providing a real-time quantitative analysis of the amount of MnO<sub>2</sub> that electrodeposits/electrodissolves during the galvanostatic cycles.

## Results and Discussion

The GLAD-ITO electrodes (1  $\mu\text{m}$ -thick film) were prepared according to the published technique<sup>24</sup> using a deposition angle of  $80^\circ$  (see Experimental section) and rapid rotation. This combination leads to growth of vertically-oriented ITO nanopillars on an underlying commercial ITO substrate (Figure 1). The nanopillars are separated from one another with a void spacing in the range of tens of nanometers throughout the entire film thickness,<sup>27</sup> attesting to a well-opened mesoporosity.<sup>28</sup> An electroactive surface area enhancement of 45 was estimated from the capacitive current determined by cyclic voltammetry (CV) at different scan rates (see Supporting Information).

The pores of the GLAD-ITO electrodes were filled with  $\text{MnO}_2$  by galvanostatic electrodeposition, controlling the amount of  $\text{MnO}_2$  through the deposition time (see experimental section). The resulting  $\text{MnO}_2$ -modified electrodes were then characterized by SEM, XPS, EDX and UV-vis absorption spectroscopy as detailed in the Supporting Information. Cross-sectional SEM and EDX images reveal that  $\text{MnO}_2$  uniformly grows inside the porosity of the GLAD structure and locally forms interwoven nanofibers (Figure 1). The top-view images in Figure 1 show that  $\text{MnO}_2$  exhibits a typical carambola-like morphology similar to that obtained from electrodeposited films on planar ITO electrodes. For the deposited charge of  $240 \text{ mC}\cdot\text{cm}^{-2}$ , the ITO nanocolumns remains clearly discernible from above (Figure 1), while at higher loads, once the pores of the GLAD ITO are filled, the  $\text{MnO}_2$  deposit continues to develop far outside the



**Figure 1 (2-columns).** Top-view and cross-sectional SEM images of  $\text{MnO}_2$  films electrodeposited on 2D ITO or 1  $\mu\text{m}$ -thick GLAD-ITO electrodes, with different  $\text{MnO}_2$  loads ranging from 0 to 400  $\text{mC}\cdot\text{cm}^{-2}$ . The orange arrow represents the 1  $\mu\text{m}$ -bar scale. The dashed yellow lines delimit the planar ITO glass substrate underneath the  $\text{MnO}_2$  film or the 3D GLAD-ITO structure. For the film loaded with 400  $\text{mC}\cdot\text{cm}^{-2}$  (rightmost images), the EDX mappings for In and Mn content are reported.

GLAD-ITO structure, making the ITO nanocolumns no longer discernable. This behavior is well evidenced in Figure 1, where a  $\sim 0.8$   $\mu\text{m}$ -thick  $\text{MnO}_2$  film is observable by both SEM and spatially-resolved EDX on top of the GLAD-ITO electrode charged at 400  $\text{mC}\cdot\text{cm}^{-2}$ . (An even thicker film, reaching  $\sim 1.6$   $\mu\text{m}$ , is observed for the electrode charged at 800  $\text{mC}\cdot\text{cm}^{-2}$ , see Figure S1D). Such a transition between filling of the GLAD-ITO pores with  $\text{MnO}_2$  and subsequent growth far beyond the GLAD-ITO structure is also identified in the galvanostatic electrodeposition curves, showing after a certain delay a sudden  $\sim 20$  mV jump in the potential. This potential jump is moreover linearly correlated with the GLAD-ITO thickness as the potential jump shifted from 150 to 90 and then 60  $\text{mC}\cdot\text{cm}^{-2}$  when the GLAD-ITO thickness decreased from 1 to 0.6 and then 0.3  $\mu\text{m}$ , respectively (Figure S1A).

In order to investigate the benefit of a 3D nanostructured current collector on the reversible conversion of  $\text{MnO}_2$  into  $\text{Mn}^{2+}$ , 1  $\mu\text{m}$ -thick GLAD-ITO electrodes were loaded with an intermediate amount of deposited charge of  $100 \text{ mC}\cdot\text{cm}^{-2}$  (or  $48.4 \mu\text{g}\cdot\text{cm}^{-2}$ ) to ensure the  $\text{MnO}_2$  was fully restricted to the interior of the porous structure. The maximal capacity stored in these  $\text{MnO}_2$ -modified electrodes was estimated from the average oxidation state (AOS) of the Mn centers, which in turn was determined from the linear correlation between the amount of electrodeposited Mn centers obtained by ICP quantification and the effective charge passed during the electrodeposition (see Supporting Information and Figure S1B for details). An AOS value of 3.86 was deduced, which is indicative of 1.86 electrons stored per Mn center. This value is in quite good agreement with the AOS of 3.75 determined by XPS analysis of the Mn(3s) peak splitting energy (Figure S1E). We thus conclude a maximal recoverable gravimetric capacity of  $574 \text{ mA}\cdot\text{h}\cdot\text{g}^{-1}$  for the full conversion of the electrodeposited  $\text{MnO}_2$ , and we define the C-rate thanks to this value (1 C corresponding to  $0.574 \text{ A}\cdot\text{g}^{-1}$ ).

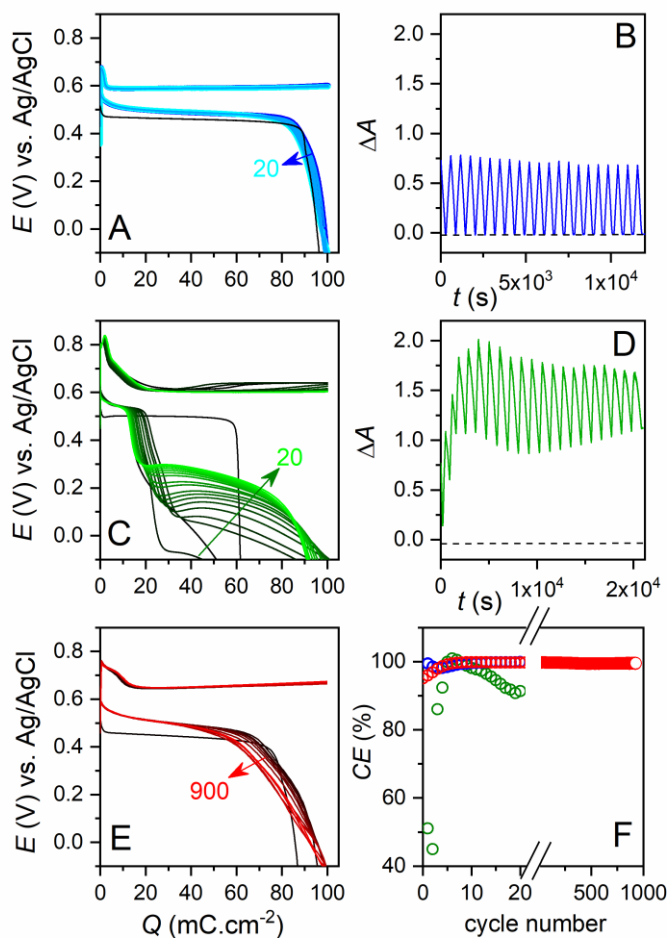
$\text{MnO}_2$ -GLAD-ITO electrodes charged at  $100 \text{ mC}\cdot\text{cm}^{-2}$  were galvanostatically cycled in buffered electrolyte and concomitantly monitored by *in-situ* UV-vis spectroscopy. The results reported in Figure 2 demonstrate the full exploitation of  $\text{MnO}_2$  when working in a 1 M acetate buffer at pH 5, containing 0.1 M  $\text{MnCl}_2$ . Indeed, full discharge of the capacity is reported with a near-perfect overlay of the first 20 galvanostatic cycles performed at  $11 \text{ A}\cdot\text{g}^{-1}$  (19 C-rate), except for the initial discharge which is associated with a slightly lower capacity. Simultaneously, the electrode absorbance oscillates evenly and stably between 0.7 and 0, underlying the excellent reversibility of the  $\text{MnO}_2$  electrodeposition/electrodissolution process. The absorbance value recorded at the end of each discharge cycle is close to the absorbance baseline (dashed line in Figure 2B), which demonstrates the complete reductive dissolution of  $\text{MnO}_2$ . The small and stable voltage hysteresis

(< 0.1 V) observed between the well-defined charge and discharge plateaus at rates lower than 11 A·g<sup>-1</sup> is indicative of a rather fast reversible conversion process, occurring under nearly thermodynamic equilibrium (at least at rates < 11 A·g<sup>-1</sup>), as defined by the following Nernst equation:<sup>7</sup>

$$E = E_{MnO_2/Mn^{2+}}^0 - 0.12 \times pH - 0.03 \times \log(a_{Mn^{2+}}) \quad (2)$$

where  $E_{MnO_2/Mn^{2+}}^0$  is the standard potential of the MnO<sub>2</sub>/Mn<sup>2+</sup> redox couple and  $a_{Mn^{2+}}$  the activity of soluble Mn<sup>2+</sup> ions. Hence, based on this equation, the highly stable charge and discharge potentials, leading to well-defined horizontal plateaus, suggest that no significant pH or Mn<sup>2+</sup> gradients develop at the electrode/electrolyte interface within the range of rates investigated. The Coulombic efficiency reported in Figure 2F starts at 98% and rapidly tends to almost 100% after a few cycles, leading to an exceptionally high gravimetric capacity  $C_g$  of 560 ± 10 mA·h·g<sup>-1</sup> deduced from absorbance and eq. S2. This capacity, close to the aforementioned maximal capacity of 574 mA·h·g<sup>-1</sup>, unambiguously demonstrates the full exploitation of the charge storage capacity that can be delivered by the present MnO<sub>2</sub>-GLAD-ITO electrode. The excellent reversibility persists over long-term cycling; over 900 cycles at 44 A·g<sup>-1</sup> (*i.e.*, 77 C), an almost constant Coulombic efficiency close to 100% is retained (*i.e.*, >99.4 % for every cycle after the 5 initial cycles) (Figure 2D).

These results differ significantly from those obtained at 2D MnO<sub>2</sub>-ITO electrodes, prepared by electrodeposition of MnO<sub>2</sub> on planar ITO electrodes with the same initial deposited charge of 100 mC·cm<sup>-2</sup>. Indeed, the data reported in Figure 2D demonstrate a significant accumulation of MnO<sub>2</sub> during the initial cycles, as attested by (i) the discharge capacities lower than 100 mC·cm<sup>-2</sup>, (ii) the CE < 90 %, and (iii) the nonzero absorbance value recorded at the end of each discharge step. The fraction of MnO<sub>2</sub> accumulated



**Figure 2 (1-column).** Galvanostatic cycling of electrodes initially charged at  $100 \text{ mC}\cdot\text{cm}^{-2}$  in a 1 M acetate buffer (pH 5) containing 0.1 M  $\text{MnCl}_2$  and 0.85 M KCl. (A) Galvanostatic curves (20 cycles from dark to light blue with the first discharge in black) of a 3D  $\text{MnO}_2$ -GLAD-ITO electrode at  $11 \text{ A}\cdot\text{g}^{-1}$  and (B) the corresponding UV-visible absorptometric traces. (C) Galvanostatic curves (20 cycles from dark to light green with the first discharge in black) of a 2D  $\text{MnO}_2$ -ITO electrode at  $7.2 \text{ A}\cdot\text{g}^{-1}$  and (D) the corresponding UV-visible absorptometric traces (the black dashed line represents the absorbance baseline). (E) Galvanostatic curves recorded at a 3D  $\text{MnO}_2$ -GLAD-ITO electrode over 900 cycles at  $44 \text{ A}\cdot\text{g}^{-1}$ . Only the following discharge/charge curves were overlaid: (black) initial discharge and (from dark red to light red) 1<sup>st</sup>, 10<sup>th</sup>, 20<sup>th</sup>, 50<sup>th</sup>, 100<sup>th</sup>, 200<sup>th</sup>, 300<sup>th</sup>, 500<sup>th</sup>, 700<sup>th</sup> and 900<sup>th</sup> cycles. (F) Evolution of the Coulombic efficiency as a function of the cycle number performed at a rate of: (green dots) 7.2, (blue dots) 11 and (red dots)  $44 \text{ A}\cdot\text{g}^{-1}$ .

after 20 cycles was roughly estimated from the absorbance value  $\Delta A$  recorded at the end of the last cycle and corresponds to *ca.*  $70 \mu\text{g}\cdot\text{cm}^{-2}$  (see Supporting Information for details). This mass, equivalent to 145% of the mass electrodeposited during each charging step, indicates that only 40% of the  $\text{MnO}_2$  is reversibly exploited. This leads to a significant loss in the gravimetric capacity, reaching only  $235 \text{ mA}\cdot\text{h}\cdot\text{g}^{-1}$  after a few cycles. These observations are in line with what we previously reported at 2D  $\text{MnO}_2$ -ITO electrodes using the same electrolyte but with lower amounts of electrodeposited  $\text{MnO}_2$ .<sup>7</sup>

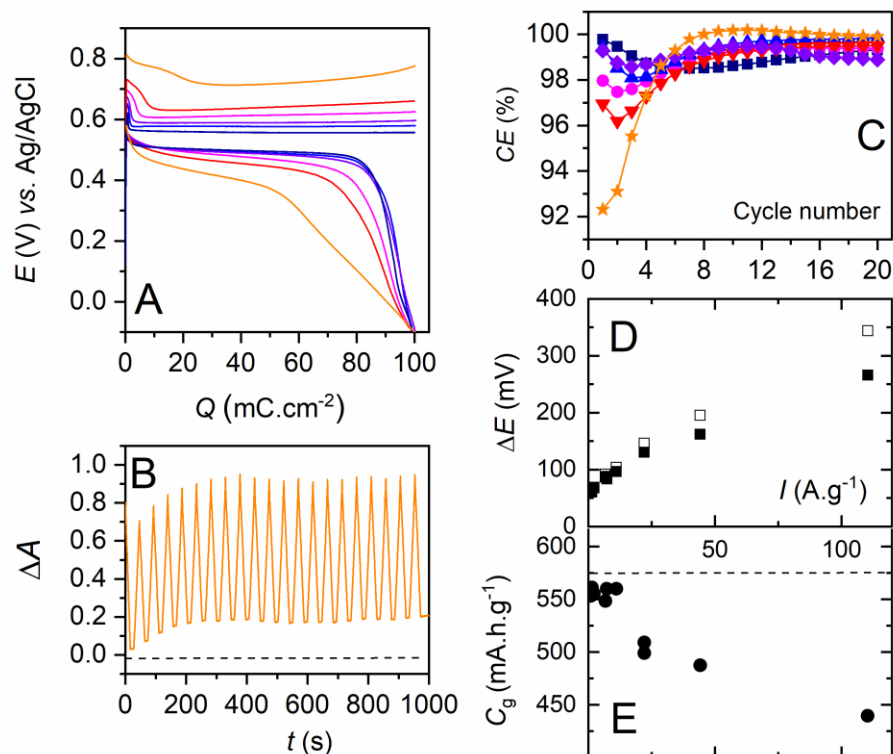
Another striking difference between the 3D  $\text{MnO}_2$ -GLAD-ITO and 2D  $\text{MnO}_2$ -ITO electrodes is the shape of the galvanostatic discharge curves, exhibiting one or two plateaus, respectively. At the  $\text{MnO}_2$ -GLAD-ITO electrode, the discharge potential centered on a well-defined value of 0.49 V is also remarkably stable until *ca.* 80% of the  $\text{MnO}_2$  is electrodisolved. *On contrario*, the discharge curves recorded at the 2D  $\text{MnO}_2$ -ITO electrode exhibit, after a few cycles, a less well-defined supplementary plateau at a much lower potential of  $\sim 0.25\text{V}$ , corresponding to roughly 80% of the total discharge process (Figure 2C). This shift in potential contributes to a huge increase in the voltage hysteresis, thereby severely affecting the charge storage energy efficiency. We previously attributed this second plateau to the formation of a more resistive fraction of  $\text{MnO}_2$  at the planar electrode, a fraction which is probably much less electrically connected to the underlying current collector.<sup>7</sup> The lack of a second plateau with the 3D  $\text{MnO}_2$ -GLAD-ITO electrode tends to confirm this assumption. It also supports the idea that the 3D nanostructured substrate facilitates the electrical wiring of  $\text{MnO}_2$  by shortening the electron transport distances across the semi-conductive  $\text{MnO}_2$ , and possibly also by strengthening the interactions between  $\text{MnO}_2$  and ITO due to the nanocolumns' roughness visible in SEM images (Figure 1). This result clearly highlights the benefit of the nanostructured electrode to facilitate the reversible

electrodissolution/electrodeposition of  $\text{MnO}_2$  into/from  $\text{Mn}^{2+}$ , and this benefit should persist as long as the conversion reaction remains within the porosity of the GLAD-ITO electrode. This latter assertion is corroborated by the cycling experiments in Figure S4 carried out with a progressive increase of the deposited charge (*i.e.*, the amount of  $\text{MnO}_2$  was increased until it grew far beyond the GLAD-ITO boundary). In the corresponding discharge curves, a second plateau at a lower potential of 0.3 V gradually emerged as the deposited charge increased. The development of this secondary plateau is also accompanied by a progressive and significant decrease in the Coulombic efficiency.

The efficiency and rate capability of the conversion process at  $\text{MnO}_2$ -GLAD-ITO electrodes was further investigated by cycling electrodes at different rates from 1.4 to 110  $\text{A}\cdot\text{g}^{-1}$  (*i.e.*, from 2.4 C to 190 C). The results gathered in Figure 3 first show that the Coulombic efficiency of the first cycles decreases as the rate increases, with initial CE values below 98% for rates  $> 22 \text{ A}\cdot\text{g}^{-1}$  (*i.e.* 38 C). Accordingly, a small fraction of poorly active  $\text{MnO}_2$  accumulates at the electrode at the fastest rate, as attested by the nonzero absorbance values  $\Delta A$  recorded at the end of the discharge steps (Figure 3B). The gravimetric capacities  $C_g$  of  $\text{MnO}_2$ -GLAD-ITO electrodes cycled at different rates are reported in Figure 3E. The data show that for rates  $< 11 \text{ A}\cdot\text{g}^{-1}$  (*i.e.*,  $< 19 \text{ C}$ ), the capacity remains almost constant at  $560 \pm 10 \text{ mA}\cdot\text{h}\cdot\text{g}^{-1}$  and close to the maximal value of  $574 \text{ mA}\cdot\text{h}\cdot\text{g}^{-1}$ , while at higher rates, the capacity decreases only slightly, remaining at  $435 \text{ mA}\cdot\text{h}\cdot\text{g}^{-1}$  for 190 C. This remarkable result demonstrates the high rate capability of this conversion process, which is quite attractive for the development of sustainable high-power storage systems. It is worth noting that as the rate increases, the voltage hysteresis also gradually increases from 60 to 340 mV, with a limited ohmic drop contribution (estimated to be  $30 \Omega$ ) which only represents 23 % of the total hysteresis at 190 C (Figure 3D). At the higher rates, we also notice an upward and downward

drift of potential during the charging and discharging steps, respectively. Based on the Nernst equation (eq. 2), we assume this arises from local pH and/or  $\text{Mn}^{2+}$  gradient changes, driven by mass transport limitations. At the lower rates, while the overall discharge curves overlap, the small increase in the voltage hysteresis results mainly from an increase of the charging potential. This behavior suggests that electrodeposition is intrinsically a slower process than electrodisolution.

Overall, these results demonstrate that the combined use of a 3D nanostructured electrode with a mild acidic buffered electrolyte allows for full exploitation of an electrodeposited film of  $\text{MnO}_2$ . Such a combination is decisive to provide fast and reversible  $\text{MnO}_2$ -to- $\text{Mn}^{2+}$  conversion, despite the multi-step mechanism, including proton-coupled electron transfer reactions as well as formation/breaking of metal-oxygen bonds.<sup>29</sup> The gravimetric capacity of  $560 \text{ mA}\cdot\text{h}\cdot\text{g}^{-1}$  we report here at pH 5.0 is the highest yet reported in mild acidic electrolytes,<sup>4</sup> and remains competitive with the value recently achieved under much stronger acidic conditions (pH  $\sim$ 1).<sup>9</sup> Furthermore, the conversion reaction can be carried out at outstandingly high C-rates, competing with the rate-performances achieved at  $\text{MnO}_2$ -based supercapacitors,<sup>14</sup> but with an incomparably greater charge storage capacity. Indeed, as illustrated in the Supporting Information, the present  $\text{MnO}_2$ -GLAD-ITO electrode in an unbuffered 1 M KCl electrolyte displayed a capacitance of  $240 \text{ F}\cdot\text{g}^{-1}$ , which is equivalent to  $60 \text{ mA}\cdot\text{h}\cdot\text{g}^{-1}$  for a potential window of 0.9 V (Figure S2), *i.e.*  $\sim$ 9-times lower than in a buffered electrolyte.

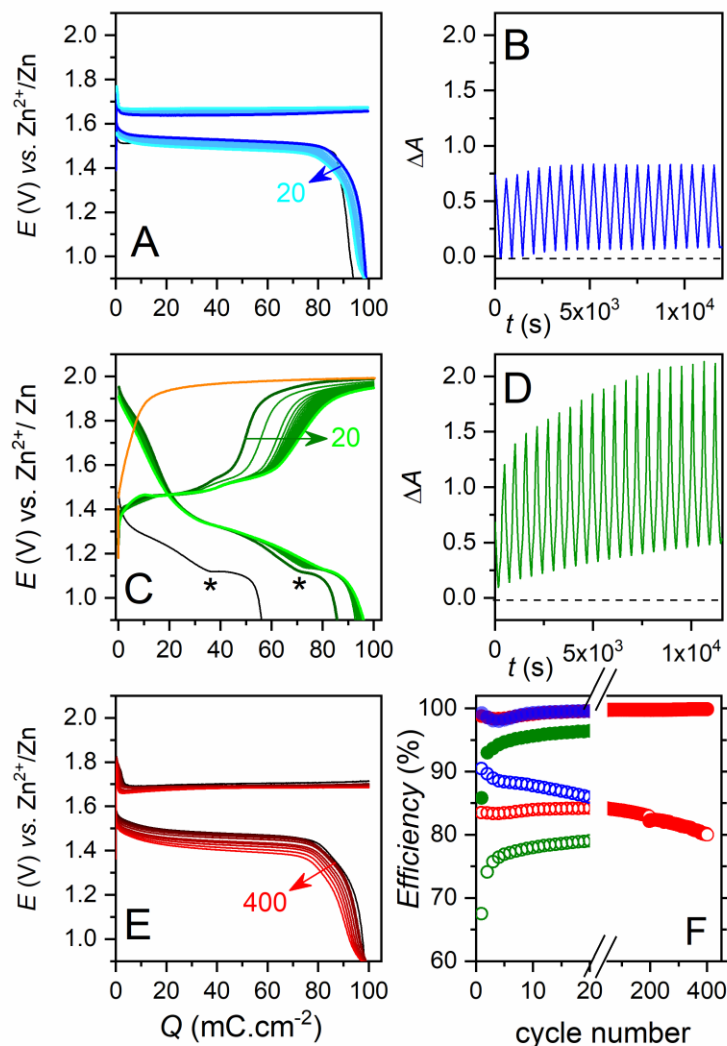


**Figure 3 (1-column).** Impact of the cycling rate over the galvanostatic cycling performances of  $\text{MnO}_2$ -GLAD-ITO electrodes (initial deposited charge:  $100 \text{ mC}\cdot\text{cm}^{-2}$ ) in 1 M acetate buffer (pH 5) along with 0.1 M  $\text{MnCl}_2$  and 0.85 M  $\text{KCl}$ . (A) 20<sup>th</sup> galvanostatic curves recorded respectively at 1.4 (navy), 7.2 (blue), 11 (violet), 22 (magenta), 44 (red) and  $110 \text{ A}\cdot\text{g}^{-1}$  (orange), and (B) the absorbance traces recorded during the 20 cycles performed at  $110 \text{ A}\cdot\text{g}^{-1}$ . (C) Coulombic efficiency as a function of the cycle number for different electrodes submitted to 20 galvanostatic cycles at a rate of: (navy) 1.4, (purple) 7.2, (blue) 11, (pink) 22, (red) 44 and (orange)  $110 \text{ A}\cdot\text{g}^{-1}$ . (D) Voltage hysteresis measured at half charge/discharge of the 20<sup>th</sup> cycle, monitored with (■) and without (□) ohmic drop correction ( $30 \Omega$ ), and (E) gravimetric capacities inferred from the absorbance measurement of the 20<sup>th</sup> galvanostatic cycle determined at different rates for  $\text{MnO}_2$ -GLAD-ITO electrodes.

The 3D MnO<sub>2</sub>-GLAD-ITO electrode was next assembled in the spectroelectrochemical cell with a Zn foil counter electrode to mimic a Zn/MnO<sub>2</sub> battery. The cell also included an Ag/AgCl reference electrode to follow the potential of both MnO<sub>2</sub> and Zn electrodes while simultaneously monitoring the MnO<sub>2</sub> absorbance. Under these conditions, the following overall charge storage conversion reaction is expected:



In addition to the acetate buffer (1.5 M, pH 5) and MnCl<sub>2</sub> (0.1 M), 0.25 M ZnCl<sub>2</sub> was added to the electrolyte, as required for the Zn-to-Zn<sup>2+</sup> conversion reaction. The electrochemical performances of the Zn/MnO<sub>2</sub> assembly are given in Figure 4. An initial series of 20 galvanostatic cycles were recorded at an intermediate rate of 7.2 A·g<sup>-1</sup> (referring here to the rate of the MnO<sub>2</sub> active material). Well-defined single charge and discharge plateaus were observed at average potential values of 1.65 and 1.50 V vs. Zn<sup>2+</sup>/Zn, respectively, which are very similar to those previously obtained in the Zn<sup>2+</sup>-free electrolyte. The voltage hysteresis slightly increases by 60 mV upon cycling, but without significantly affecting the good energetic efficiency (*EE*), which remains higher than 86 % over the 20 cycles (blue dots in Figure 4F). Remarkably, after a few preconditioning cycles, the coulombic efficiency remains over 99 %, and from the residual absorbance of the cathode at the end of the discharge steps, we can conclude that only a very small amount of a less active fraction of MnO<sub>2</sub> accumulates, estimated to 6.5 μg·cm<sup>-2</sup>, and mainly arising within the first few cycles. Accordingly, the MnO<sub>2</sub> gravimetric capacity that can be fully exploited here is 500 mAh·g<sup>-1</sup>, slightly less than in the absence of Zn<sup>2+</sup> but much higher than has previously been reported for mild aqueous Zn/MnO<sub>2</sub> batteries.<sup>4</sup> Finally, the long-term cyclability of this aqueous Zn/MnO<sub>2</sub> cell configuration was confirmed through the near absence of capacity fading over 400 cycles at 20.6 A·g<sup>-1</sup> (*i.e.*, 36 C, Figure 4E), with a Coulombic and an energetic efficiency that



**Figure 4 (1-column).** Galvanostatic cycling performances of the Zn foil/MnO<sub>2</sub>-GLAD-ITO assembly (initial charge 100 mC·cm<sup>-2</sup>) in pH 5 degassed electrolytes containing: (A, B, E) 1.5 M acetate buffer + 0.1 M MnCl<sub>2</sub> + 0.25 M ZnCl<sub>2</sub>, and (C, D) 0.25 M ZnCl<sub>2</sub> + 0.1 M MnCl<sub>2</sub> + 0.85 M KCl. The potentiometric (A, C) and UV-visible absorptometric (B, D) traces were monitored concomitantly at a rate of 7.2 A·g<sup>-1</sup> over 20 cycles with the initial discharge in black and the next 20 cycles from dark to light (either blue or green). (E) Galvanostatic curves recorded over 400 cycles at a rate of 20.6 A·g<sup>-1</sup>. Only the following discharge/charge curves were overlaid, from dark to light red: 1<sup>st</sup>, 10<sup>th</sup>, 20<sup>th</sup>, 30<sup>th</sup>, 50<sup>th</sup>, 70<sup>th</sup>, 100<sup>th</sup>, 150<sup>th</sup>, 200<sup>th</sup>, 250<sup>th</sup>, 300<sup>th</sup>, 350<sup>th</sup> and 400<sup>th</sup> cycle.

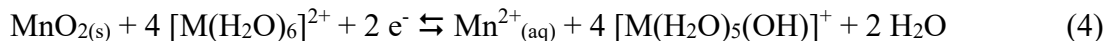
(F) Evolution of the (filled dots) Coulombic efficiency and (empty dots) energetic efficiency upon cycling the electrode at a rate of: (blue and green)  $7.2$  and (red)  $20.6 \text{ A}\cdot\text{g}^{-1}$ , respectively.

rapidly stabilize at  $99.7 \pm 0.2 \%$  and  $82.6 \pm 1.3 \%$ , respectively (red dots in Figure 4F). These results clearly demonstrate that the excellent performances of the  $\text{MnO}_2$ -GLAD-ITO electrodes are conserved in a  $\text{Zn}/\text{MnO}_2$  assembly, and that the addition of  $\text{Zn}^{2+}$  in the buffered aqueous electrolyte does not significantly interfere with the reversible  $\text{MnO}_2$ -to- $\text{Mn}^{2+}$  conversion reaction. This thus paves the way to the design of high-performance  $\text{Zn}/\text{MnO}_2$  batteries in non-corrosive mild aqueous electrolytes.

In order to demonstrate the great benefit of using a buffered electrolyte in the aforementioned experiments, the  $\text{Zn}$  foil/ $\text{MnO}_2$ -GLAD-ITO assembly was cycled in an unbuffered aqueous electrolyte (adjusted to pH 5) containing only the inorganic salts required for the conversion reaction (*i.e.*,  $0.1 \text{ M MnCl}_2$  and  $0.25 \text{ M ZnCl}_2$  along with  $0.85 \text{ M KCl}$ ). The electrochemical performances recorded at  $7.2 \text{ A}\cdot\text{g}^{-1}$  are reported in Figure 4C. First, it is worth noting that both the Coulombic and the energetic efficiency are significantly deteriorated as compared to those previously obtained in a buffered electrolyte, remaining below  $95 \%$  and  $79 \%$ , respectively, over the 20 cycles (green dots in Figure 4F). Still, the reversible conversion mechanism is supported by the absorbance change monitored at the cathode, certifying the reversible electrodisolution/electrodeposition of  $\text{MnO}_2$ . The absorbance measurements also testify to a significant accumulation of a less active form of  $\text{MnO}_2$ , estimated to be  $37 \mu\text{g}\cdot\text{cm}^{-2}$  after 20 cycles (*i.e.*,  $76 \%$  of the mass deposited during each charging step), leading to a significant loss in the  $\text{MnO}_2$  exploitation and consequently to a lower gravimetric capacity of  $310 \text{ mA}\cdot\text{h}\cdot\text{g}^{-1}$ .

It is important to keep in mind that in the absence of acetate buffer, the available proton donors are the hexaquo complexes  $[\text{Zn}(\text{H}_2\text{O})_6]^{2+}$  and  $[\text{Mn}(\text{H}_2\text{O})_6]^{2+}$  resulting from the solvation of their

parent divalent inorganic salts (here  $\text{ZnCl}_2$  and  $\text{MnCl}_2$ ). These complexes are characterized by a weak Brønsted acidity with a  $\text{p}K_{\text{a}}$  value of 9.0 and 10.6, respectively.<sup>23</sup> As we have previously demonstrated,<sup>7</sup> both complexes can act as proton donors to assist the electrodisolution of  $\text{MnO}_2$  into  $\text{Mn}^{2+}$  according to the following electrochemical reaction:



where M is either Zn or Mn. This is typically what we observed in Figure 4C, where, after a few cycles, the galvanostatic discharges lead to a similar areal capacity than in the 1.5 M acetate buffer media, but with discharge curves of very different shapes. This striking difference can be rationalized through the pH-dependent Nernst eq. 2 associated with reaction 4. During the electrodisolution, protons brought by the hexaaquo complexes at the electrode/solution interface are rapidly consumed to ensure the conversion of  $\text{MnO}_2$  into  $\text{Mn}^{2+}$ , resulting in the local production of the conjugated bases  $[\text{Zn}(\text{H}_2\text{O})_5\text{OH}]^+$  and  $[\text{Mn}(\text{H}_2\text{O})_5\text{OH}]^+$ . Consequently, the local pH increases and the discharge potential decreases. Once the local pH is sufficiently basic, the doubly deprotonated neutral forms of  $[\text{Zn}(\text{H}_2\text{O})_6]^{2+}$  and  $[\text{Mn}(\text{H}_2\text{O})_6]^{2+}$  (*i.e.*,  $\text{Zn}(\text{OH})_2$  and  $\text{Mn}(\text{OH})_2$ ) precipitate, thereby stabilizing the local pH, an effect that is observed through the appearance of a stable plateau at the end of the discharge curves (the beginning of this plateau is indicated by an asterisk on Figure 4C).<sup>22</sup> Such precipitation of insoluble hydroxides over the  $\text{MnO}_2$  cathode most likely contributes to a loss in the conversion efficiency, probably by slowing down the ongoing reductive dissolution of  $\text{MnO}_2$ . Evidence for the precipitation of such zinc hydroxides has been previously reported in several studies and also related to a local pH.<sup>3,18–22</sup> However, none of these studies explicitly identified the proton source, preventing a clear explanation to the local pH changes and thus the associated precipitation of zinc hydroxides, both governed by the  $\text{p}K_{\text{a}}$ s and local activities of the weak acid and conjugated base acting as proton donor/acceptor.

Concerning the charging curves, which involve  $\text{MnO}_2$  electrodeposition with the concomitant local release of several equivalents of protons, the first plateau observed at 1.45 V (Figure 4C) suggests a stabilization of the local pH at an intermediate mild acidic value. This effect can be rationalized from the dynamic equilibrium that is expected to persist through the continuous neutralization of the protons released by the Brønsted bases which are generated during the previous discharge step (and which include the precipitated hydroxides). This interpretation is further supported by the absence of a similar plateau when the galvanostatic charge is immediately applied to a  $\text{MnO}_2$ -GLAD-ITO electrode without prior discharge (orange curve, Figure 4C), leading to a direct rise of the charging potential up to a plateau at  $\sim 2$  V vs.  $\text{Zn}^{2+}/\text{Zn}$ , which is close to the charging potential previously reported for an acidic  $\text{Zn}/\text{MnO}_2$  battery (*i.e.*, 2.2 V in the presence of a 0.1 M  $\text{H}_2\text{SO}_4$  electrolyte).<sup>9</sup> This result is thus indicative of the strong pH gradients that develop during the electrodeposition of  $\text{MnO}_2$  from an unbuffered electrolyte.

Besides the demonstration of the beneficial effect of buffered electrolytes on the stabilization of the potentials of  $\text{MnO}_2$  electrodeposition and electrodisolution, the present work also provides a clear explanation of the good performances recently achieved for a  $\text{Zn}/\text{MnO}_2$  battery using an aqueous unbuffered electrolyte containing zinc and manganese acetate salts.<sup>30</sup> While the authors focus on the coordinating role of the acetate ions to explain the high performances they obtained and the low  $\text{MnO}_2$  electrodeposition potential they observed ( $\sim 1.8$  V vs.  $\text{Zn}^{2+}/\text{Zn}$ ), the present results rather suggest that the increased performance is due to a local buffering effect. Indeed, the protons locally released during the electrodeposition are neutralized by the acetate ions present in the electrolyte, generating acetic acid in dynamic equilibrium with the remaining acetate ions. In the following discharge step, this acetic acid thus behaves as the proton donor to efficiently assist the reductive electrodisolution of  $\text{MnO}_2$ . It is worth noting that significant shifts of the charging

and discharging potentials were reported in such unbuffered aqueous electrolytes, which most likely arises from large variations in the local concentrations of acetate and acetic acid, and thus in the local pH.

## Conclusion

In the present work, we demonstrate the beneficial combination of a nanostructured conductive 3D substrate and a buffered electrolyte to fully exploit the reversible, two-electron  $\text{MnO}_2$ -to- $\text{Mn}^{2+}$  conversion mechanism in mild acidic conditions. The corresponding cathode is characterized by a high gravimetric capacity ( $560 \text{ mA}\cdot\text{h}\cdot\text{g}^{-1}$ ), high rate capability ( $435 \text{ mA}\cdot\text{h}\cdot\text{g}^{-1}$  at 190 C), low charge/discharge hysteresis (thus high energetic efficiency) and high cyclability (up to 900 cycles with a CE > 98%). Such performances are preserved in a Zn/ $\text{MnO}_2$  cell configuration, outperforming all the mild aqueous Zn/ $\text{MnO}_2$  assemblies so far described, with a highly stable potential of 1.5 V over almost the complete discharge, an unprecedented gravimetric capacity of  $500 \text{ mA}\cdot\text{h}\cdot\text{g}^{-1}$  at 12 C and a stable Coulombic efficiency of 99.7 % over 400 cycles at 36 C.

These great performances arise from properly balancing the electrolyte composition (to avoid mass transport limitation) and the  $\text{MnO}_2$  mass loading regarding both the surface enhancement and the porosity of the nanostructured conductive 3D substrate (to avoid long-range electron transport throughout the semiconductive  $\text{MnO}_2$  film and thus ohmic drop issues). The present demonstration was performed using transparent model GLAD-ITO electrodes, allowing for *in-situ* monitoring of the conversion process. These model electrodes, however, are unsuitable for charge storage applications, and therefore, further developments require scaling-up the conversion process with inexpensive, high surface area conductive substrates to get beyond the low gravimetric capacities of mild aqueous Zn/ $\text{MnO}_2$  batteries.

## Experimental Section

**Chemicals.** HNO<sub>3</sub> (Suprapur, 65%), acetic acid (Reagent plus, > 99%), KOH, HCl (Normapur, 37%), KCl (GR for analysis), ethanol absolute (EMSURE) and ZnCl<sub>2</sub> were purchased from Sigma-Aldrich/Merck. MnCl<sub>2</sub> tetrahydrate (99%) was purchased from Alfa Aesar. Acetone (Normapur) and chloroform (Normapur) were purchased from VWR Chemicals.

**GLAD-ITO Mesoporous Electrodes.** Porous ITO thin films were prepared by the glancing angle deposition (GLAD) method followed by thermal treatment as previously described.<sup>24</sup> Briefly, nanostructured ITO films were deposited from ITO evaporant (Cerac, 91:9 In<sub>2</sub>O<sub>3</sub>/SnO<sub>2</sub> 99.99% pure) in an electron-beam physical vapor deposition system (Axxis, Kurt J Lesker) on ITO-coated glass substrates (8-12 Ω/□, Delta Technologies Ltd.). Throughout the deposition, substrates were maintained at an 80° angle with respect to impinging evaporant flux, while constantly rotating as a feedback-controlled function of the deposition rate. The film thickness was adjusted between 0.3 and 1 μm. Following deposition, the GLAD-ITO samples were thermally annealed in a two stage process, first under air at 500 °C and subsequently under 5% H<sub>2</sub>/Ar flow at 375 °C, to improve and stabilize the optical and electrical properties. For such deposition conditions, the film porosity was previously estimated to be 0.5 and its density to be 4 g·cm<sup>-3</sup>.<sup>24</sup> Prior to the electrochemical experiments, the GLAD-ITO electrodes were cleaned by soaking them successively in chloroform, acetone, and ethanol, each time for 30 min at 50°C. After the electrodes were left to dry, a geometric area of 0.50 ± 0.04 cm<sup>2</sup> (N = 40) was delimited by depositing an insulating layer of nail polish.

**Preparation of the MnO<sub>2</sub>-coated GLAD-ITO electrodes.** The deposition of MnO<sub>2</sub> within the 3D structure of GLAD-ITO electrodes was performed by galvanostatic electrodeposition using a standard three-electrode cell configuration at room temperature (23 ± 3 °C) and a multichannel potentiostat/galvanostat (VSP model, BioLogic instrument). An SCE and Pt-grid were used as

reference (+0.244 V vs. NHE) and counter electrode, respectively. For electrodeposition, freshly cleaned GLAD-ITO electrodes were placed in 7 mL of a quiescent acetate buffer (1 M, pH 5.0) containing 0.1 mM MnCl<sub>2</sub> and 0.85 M KCl. After preconditioning by cyclic voltammetry (CV) from 0.35 to 0.75 V (4 cycles) at 100 mV·s<sup>-1</sup>, galvanostatic electrodeposition at 300 μA·cm<sup>-2</sup> (normalized to the geometric electrode area) was performed for a duration leading to final deposited charges,  $Q$ , ranging from 50 to 800 mC·cm<sup>-2</sup>. After electrodeposition, the MnO<sub>2</sub>-modified electrodes were soaked for a few minutes in purified water and left to dry at room temperature. For each electrode, the initial amount of electrodeposited MnO<sub>2</sub> ( $m_{MnO_2}^i$  in μg·cm<sup>-2</sup>) was estimated from the following relationship:

$$m_{MnO_2}^i = (0.484 \pm 0.008) \times Q \quad (4)$$

Further details on the characterization of these MnO<sub>2</sub>-coated GLAD-ITO electrodes by UV-visible absorption spectroscopy, XPS and ICP are reported in the Supporting Information.

**Aqueous electrolyte compositions.** Aqueous electrolytes with the following chemical composition were prepared in purified water: (i) 1 M acetate buffer (pK<sub>a</sub> = 4.76) at pH 5.0 (prepared from a 2 M acetic acid solution adjusted to the desired pH with 2 M KOH) along with 0.1 M MnCl<sub>2</sub> and 0.85 M KCl ( $I = 1.9$  M), (ii) 1.5 M acetate buffer at pH 5.0 along with 0.1 M MnCl<sub>2</sub> and 0.25 M ZnCl<sub>2</sub> ( $I = 2.3$  M), (iii) 0.25 M ZnCl<sub>2</sub> along with 0.1 M MnCl<sub>2</sub> and 0.85 M KCl adjusted to pH 5.0 with 1 M HCl ( $I = 1.9$  M), (iv) 1 M KCl adjusted to pH 5.0 with 1 M HCl ( $I = 1$  M).

**Spectroelectrochemistry.** Spectroelectrochemical experiments were performed in a quartz UV-visible cell modified to accommodate three electrodes with an electrolyte volume of 1.2 mL. The counter electrode was a Pt grid (0.06 mm wire diameter, 0.25 mm nominal space, Goodfellow) or a zinc foil (0.35 mm thickness, Goodfellow) and the reference electrode was a Dri-Ref

Ag/AgCl/KCl<sub>sat</sub> electrode (+0.2 V vs. NHE, WPI Instruments). Unless otherwise stated, all reported potentials are quoted against this reference electrode. The UV-visible absorption spectra were recorded in transmission mode using an HR-2000+ spectrometer (Ocean Optics) controlled by the SpectraSuite software. Spectra were obtained by averaging 50 individual spectra recorded with an integration time of 40 ms. For the galvanostatic experiments, the electrochemical cell was controlled by a VSP BioLogic potentiostat interfaced with the EC-Lab 11.3 software. A period of 10 s at the open circuit potential was systematically added at the end of each discharge during the galvanostatic cycling experiments to allow relaxation of the potential.

All gravimetric intensities ( $A \cdot g^{-1}$ ) were calculated from the current density ( $mA \cdot cm^{-2}$ ) applied to the electrode and the expected electrodeposited mass of MnO<sub>2</sub>, deduced from eq. 4. The Coulombic efficiency ( $CE$ ), energetic efficiency ( $EE$ ), and gravimetric capacity ( $C_g$  in  $mA \cdot h \cdot g^{-1}$ ) were calculated using the following equations:

$$CE = \frac{Q_{i,disch}}{Q_{i,ch}} ; \quad EE = \frac{E_{i,disch}}{E_{i,ch}} ; \quad C_g = \frac{1000}{3.6} \frac{Q_{i,disch}}{m_{ch} + m_{acc}} \quad (5)$$

where  $Q_{i,ch}$  and  $Q_{i,disch}$  are the areal charging and discharging capacities of the  $i$ -th cycle in  $mC \cdot cm^{-2}$ ,  $E_{i,ch}$  and  $E_{i,disch}$  the corresponding charging and discharging energy densities in  $W \cdot h \cdot cm^{-2}$  determined from the product of  $Q$  and the average charge/discharge voltages,  $m_{ch}$  the areal MnO<sub>2</sub> mass deposited during the charging step (*i.e.*,  $48.4 \mu g \cdot cm^{-2}$  for a constant charge of  $100 mC \cdot cm^{-2}$ ), and  $m_{acc}$  the total areal inactive MnO<sub>2</sub> mass accumulated at the end of the experiment (the latter being determined either by ICP analysis or from the absorbance of the electrode after discharge).

**Film characterization.** Scanning electron microscopy was performed XXX EDX mapping.... XPS spectra were recorded using a K-Alpha+ system (ThermoFisher Scientific, East-Grinstead, UK) fitted with a micro-focused and monochromatic Al K $\alpha$  X-ray source (1486.6 eV, spot size of 400  $\mu m$ ). The pass energy was set to 150 and 40 eV for the survey and the narrow high resolution

regions, respectively. The spectra were calibrated against the (C—C/C—H) C(1s) component set at 285 eV. The chemical composition was determined using the manufacturer's sensitivity factors within the Avantage software (version 5.977). The average oxidation state (AOS) of the Mn centers in the electrodeposited MnO<sub>2</sub> thin film was estimated on the basis of the XPS Mn(3s) peak splitting energy ( $\Delta BE$ ) and using the following correlation:<sup>31,32</sup>

$$AOS = 8.95 - 1.13 \times \Delta BE \text{ (eV)} \quad (6)$$

The amount of MnO<sub>2</sub> electrodeposited on ITO was analyzed by inductively coupled plasma atomic emission spectrometry (ICP-AES; Thermo Scientific iCAP 6300 ICP spectrometer) after dissolution of the MnO<sub>2</sub> film in concentrated nitric acid under ultrasonication and then dilution with purified water to have a final 6.5% v/v nitric acid concentration.

## ASSOCIATED CONTEXT

### Supporting information

Elaboration and characterization of the as-prepared MnO<sub>2</sub>-GLAD-ITO electrodes (Galvanostatic curves, Absorbance and ICP quantification, XPS analysis and capacitive determination), Figures S1-S5.

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### **Authors Contributions**

The manuscript was written through contributions of all authors. All authors have given approval to the final version of the manuscript

### **Conflicts of interest**

The authors declare no conflicts of interest.

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## Table of Content – TOC illustration

