NRC Publications Archive Archives des publications du CNRC

The second expansion cycle in ultramicrocellular foams

Nawaby, A. V.; Handa, Y. P.

This publication could be one of several versions: author's original, accepted manuscript or the publisher's version. /
La version de cette publication peut être l'une des suivantes : la version prépublication de l'auteur, la version
acceptée du manuscrit ou la version de l'éditeur.

Publisher's version / Version de l'éditeur:

Cellular Polymers, 22, 4, 2003

NRC Publications Record / Notice d'Archives des publications de CNRC:

<https://nrc-publications.canada.ca/eng/view/object/?id=811705c8-aaf8-4276-902c-842b5e64f6e9>

<https://publications-cnrc.canada.ca/fra/voir/objet/?id=811705c8-aaf8-4276-902c-842b5e64f6e9>

Access and use of this website and the material on it are subject to the Terms and Conditions set forth at

<https://nrc-publications.canada.ca/eng/copyright>

READ THESE TERMS AND CONDITIONS CAREFULLY BEFORE USING THIS WEBSITE.

L'accès à ce site Web et l'utilisation de son contenu sont assujettis aux conditions présentées dans le site

<https://publications-cnrc.canada.ca/fra/droits>

LISEZ CES CONDITIONS ATTENTIVEMENT AVANT D'UTILISER CE SITE WEB.

Questions? Contact the NRC Publications Archive team at

PublicationsArchive-ArchivesPublications@nrc-cnrc.gc.ca. If you wish to email the authors directly, please see the first page of the publication for their contact information.

Vous avez des questions? Nous pouvons vous aider. Pour communiquer directement avec un auteur, consultez la première page de la revue dans laquelle son article a été publié afin de trouver ses coordonnées. Si vous n'arrivez pas à les repérer, communiquez avec nous à PublicationsArchive-ArchivesPublications@nrc-cnrc.gc.ca.

The Second Expansion Cycle in Ultramicrocellular Foams[†]

A. Victoria Nawaby¹ and Y. Paul Handa²

¹Institute for Chemical Process and Environmental Technology, National Research Council of Canada, Ottawa, Ontario, Canada K1A 0R6. ²Pactiv Corporation, Technology Center, 2651 Brickyard Road, Canandaigua, New York 14424-7990

Received: 19 March 2003 Accepted: 4 July 2003

SUMMARY

Ultramicrocellular PMMA foams made from the low temperature rubbery phase, obtained by saturating the polymer with CO₂ at 0°C and 34 atm, was subjected to a second expansion cycle by heating it rapidly to temperatures in the range 30 to 120°C. The blowing agent for the secondary expansion was either the residual CO₂ in the foam at about 19 wt% level or fresh CO₂ re-equilibrated at 0°C and 34 atm to a loading level of about 29 wt%. In the former case, the second expansion cycle led to lower foam densities whereas in the latter case it led to stretching and re-orientation of the cell walls with no significant gain in further foam density reduction or cell density increase.

INTRODUCTION

It is well known that compressed gases such as CO₂ and N₂ can dissolve to considerable extent in polymers to induce cell nucleation and growth on depressurization. The cellular morphology thus obtained is often in the 10–100 µm range. Two processes are often used to generate such structures. In the continuous extrusion process, the molten polymer is directly injected with compressed gas, followed by dissolution and a final pressure and temperature decrease to generate the cellular structure. In the batch solid-state extrusion process, the polymer is saturated with the compressed gas under appropriate temperature and pressure conditions, followed by either rapid depressurization or first slowly decreasing the pressure and then quickly heating the polymer-gas solution to a temperature above the plasticized glass transition temperature, T_g . Generally, the closed cell morphologies with cell diameter in the range 1–100 µm and a cell density about 10⁸ cells/cm³ are termed microcellular foams.

[†]Correspondence to: A. V. Nawaby (victoria.nawaby@nrc.ca).

[†]Issued as NRCC No. 46442

The cellular structures with a diameter in the range 0.01-1 μm and a cell density in excess of 10^{12} cells/ cm^3 are termed ultramicrocellular foams⁽¹⁾.

CO_2 in particular is considered a desirable blowing agent due to its physical properties and benign nature. This gas near or above its critical point can dissolve in large enough quantities to cause an appreciable reduction in the T_g of the polymer-gas system⁽²⁾. For poly(methyl methacrylate), PMMA, CO_2 is an excellent plasticizer causing a T_g depression which is not linearly dependent on the gas pressure as generally is the case but, instead, the system exhibits a retrograde behavior^(1,3,4) whereby two transitions under a constant gas pressure are observed: a rubber-to-glass transition at a lower temperature ($T_{g,l}$), and a glass-to-rubber transition at a higher temperature ($T_{g,h}$). The existence of $T_{g,l}$ is due to the higher solubility of the gas in the polymer at lower temperatures, and heating the system at a constant pressure results in some gas loss from the polymer giving a rubber-to-glass transition accompanied by generation of microcellular morphology. On further heating at the same constant pressure results in the usual glass-to-rubber transition at $T_{g,h}$, and to the generation of ultramicrocellular morphology due to a much higher cell nucleation rate. Ultramicrocellular foams with an average cell size of 0.35 μm and cell density of 10^{13} cells/ cm^3 were produced by saturating PMMA with CO_2 in the liquid or sub-critical state^(3,4). The reported low temperature/pressure process offers better control on cell growth and gives finer morphologies as compared to those reported in the literature⁽⁵⁾.

The evolution of ultramicrocellular foams has created an interest in exploring pathways to generate morphologies beyond the sub-micron level. While searching for newer processing windows using the patented low temperature foaming process^(3,4), it was observed that the foams exhibited significant mass change over time due to loss of CO_2 . The availability of this considerable amount of CO_2 in the foam, which we will refer here as the primary foam, offers the possibility to use this extra gas to re-foam the ultramicrocellular morphology and obtain smaller cell sizes or lower density. The re-foamed morphology is therefore referred to as secondary foam.

In conventional foaming processes, for example in the case of polystyrene (PS), secondary foaming is commonly practiced. The extruded PS foams can normally retain about 50-90% of the physical blowing agent. As foam ages and air permeates into the cells, the total cell pressure (from the permeated air and residual blowing agent) during a converting stage, such as thermoforming, can be much higher than atmospheric and causes a further expansion of the cells and hence secondary foaming. Another variant of the secondary foaming process has been recently reported^(6,7) whereby density of a thermoplastic

foam is further reduced by resaturating with a compressed gas such as CO₂ and subjecting the foam-gas solution to another expansion cycle.

In this paper we will explore whether the ultramicrocellular foams produced from the retrograde phase can be subjected to secondary foaming and its effect on the resulting morphological characteristics.

EXPERIMENTAL

PMMA sample used had a T_g of 95 °C, $M_w = 108,500$, and $M_n = 56,700$. It was compression molded into sheets of about 1.25 mm in thickness. Bone dry CO₂ was used.

Primary PMMA foams were prepared by saturating the polymer with CO₂ at 0°C and 34 atm for 24 hours and subsequently heating in a water bath at 50°C. Secondary foams were prepared utilizing the CO₂ left in the sample after aging under ambient conditions from 2 to 14 days, and then heating to 120°C. The secondary foams were also prepared by placing the primary foam in a vacuum oven at 30°C for 3 days, then re-saturating with CO₂ at the above conditions for 24 hours and subsequently foaming in the range 30 to 120°C. Primary PMMA foam samples after the vacuum step were also saturated with N₂ gas at 24°C and 54 atm to investigate the effect of gas type on secondary foaming.

Desorption kinetic studies on the primary foam samples were carried out using a high-precision gravimetric technique (CAHN D110 microbalance)⁽⁸⁾. A sample with dimensions 1.5x0.5x0.5 cm and weighing 0.4 g was placed in the balance and the entire system evacuated. The amount of gas loss as a function of time at various temperatures in the range 14 to 55°C was monitored until no further mass changes was observed. Foam densities were determined by measuring the mass in air and in water.

RESULTS AND DISCUSSION

During the foaming process, initially the pressure of CO₂ within the matrix is higher than the ambient. On aging at a given temperature, the concentration gradient results in diffusion of CO₂ out of the matrix until an equilibrium with the surroundings is established. Even with the CO₂ at 1 atm inside the cells, the foam matrix acts as a gas reservoir, considering (as shown below) the amount of CO₂ present in the cells and that dissolved in the polymer matrix. A typical desorption curve under ambient conditions is shown in Figure 1. The total

amount of gas given off by the primary foam is about 19 wt%, and represents a retention of about 65% of the initial amount of the blowing agent dissolved in the polymer before foaming. As expected, the total amount of gas given off was the same irrespective of the desorption temperature except that the desorption rates became more rapid with increasing temperature. For example at 14°C equilibrium was reached after 21 days as compared to 6 days at 55°C. The analysis of the kinetic data using the hybrid model⁽⁸⁾ gives desorption diffusion coefficients in the range 2.5 to 3.9×10^{-7} cm²/s over the temperature range of 14 to 55°C.

In the microcellular foaming process, the morphology obtained is directly dependent on the amount of dissolved gas and the foaming temperature⁽¹⁾. This implies that the amount of gas left in the resulting foam is also a function of the cellular morphology. This indeed was found to be the case. As seen in Figure 2, a correlation exists between the total amount of gas desorbed from the primary PMMA foam and the primary foam characteristics, and is similar in nature as the correlation with the amount of dissolved gas⁽¹⁾. Cell density measurements were carried out using the method as described previously⁽⁹⁾. Cell sizes were determined using the image analysis software Image-Pro from

Figure 1 Change in mass of primary PMMA foam sample under ambient conditions

Figure 2 Cell density and cell size of the primary foam samples plotted against the amount of residual gas in the sample

Cybernetics and SEM photographs of the foam samples. As shown in Figure 2, the amount of residual gas in the sample gas corresponds to the foaming temperature – *i.e.* the higher the foaming temperature, the less gas is available for desorption, and the accompanying morphology is reflected in smaller cell size and higher cell density.

Results on the secondary foams obtained after aging the primary foam samples for various times followed by rapidly heating the sample to 120°C are shown in Figure 3 where reduction in density of the primary foam is plotted against the time it was aged before re-foaming. It is noted from Figure 1 that the majority of the gas loss occurs in the first three days with the rest exhibiting a gradual exponential decay. Accordingly, the largest density reduction achieved was 0.38 g/cm³ when a freshly made primary foam sample with a density of 0.50 g/cm³ was aged for 2 days and subsequently foamed to give secondary foam with a density of 0.12 g/cm³. With further aging, the density reduction achieved decreased and eventually leveled off for samples aged 6 days or more. This is also reflected in that no change in the cell size or cell density was evident in the SEM analysis on the secondary foam sample made after aging for more than 6 days. On the other hand, as shown in Figure 4, a

Figure 3 Density reduction achieved after aging the primary foam for various periods and then rapidly heating it to 120°C

Figure 4 Microphotographs of PMMA foams: a) primary foam prepared at 100°C, b) secondary foam prepared by aging the primary foam for 2 days and then rapidly heating it to 120°C

significant change in the cell size was observed when primary foam made at 100°C (Figure 4a) was aged for 2 days and then subsequently heated to 120°C (Figure 4b).

The primary foams were also re-foamed by subjecting the samples to a second saturation cycle using CO₂ and N₂ and a second expansion cycle in the temperature range 30 to 120°C. Since, as noted above, the primary foams prepared at 50°C contained a significant amount of CO₂ within the morphology, the samples were first left in the vacuum oven at about 30°C for 3 days prior to re-saturation. The resultant secondary foam densities are shown in Figure 5. The secondary foams prepared with a second saturation step using CO₂ exhibit the same trend and are within experimental error as the primary foam densities. The primary foam densities as previously reported by Handa and Zhang⁴ seem to level off in the foaming temperature range of 80 to 100°C whereas the secondary foam densities continue to decrease up to 120°C. The densities of the secondary foam prepared with N₂ remain constant at about 0.45 g/cm³, which is close to the density of primary foam prepared at 50°C. This is due to the fact that the solubility of N₂ is much lower than that of CO₂ and thus does not contribute to further expansion of the matrix until at higher temperatures

Figure 5 Primary and secondary foam densities using CO₂ and N₂ as the blowing agents for the second expansion cycle

where density reduction is observed once the foaming temperature surpasses the T_g of the system.

Figure 6 shows microphotographs of the secondary foams prepared at 120°C with CO₂ and N₂ gases. The re-saturation with CO₂ and re-foaming of the primary foam, Figure 8a, results in reorientation of the cell walls due to the high solubility of this gas in the polymer at lower temperatures and the severe plasticization of the matrix. Such relaxation is not available in the case of N₂ due to the rather limited solubility of N₂ and becomes possible only when the system approaches the nominal T_g of the polymer.

CONCLUSIONS

It was found that the freshly prepared ultramicrocellular foams contain enough residual blowing agent (about 19 wt%) that they can be subjected to a second expansion cycle to give morphologies with lower density, provided the secondary foaming is done at temperatures higher than those used during the primary foaming and that this operation is performed within 48 hours. Conversely, the primary foams can be first totally degassed, re-saturated with the blowing agent, and foamed again. Such a secondary foaming cycle leads to re-orientation of the primary cells without any significant density reduction.

ACKNOWLEDGEMENT

The authors thank Mr. Gerry Pleizier for assistance with the SEM work.

Figure 6 Microphotographs of secondary PMMA foams prepared at 120°C: a) with CO₂, b) with N₂

REFERENCES

1. Handa, Y. P. and Zhang, Z. *J. Polym. Sci.: Part B: Polym. Phys.* 2000, **38**, 716.
2. Handa, Y. P., Lampron, S., and O'Neill, M. L. *J. Polym. Sci.: Part B: Polym. Phys.* 1994, **32**, 2549.
3. Handa, Y. P. and Zhang, Z. US Patent No. 5,955,511, September 21, 1999.
4. Handa, Y. P., Zhang, Z., and Wong, B. *Cellular Polymers* 2001, **20**, 1.
5. Goel, S. and Beckman, E. J. *Polym. Eng. Sci.* 1994, **34**, 1148.
6. Francis, P. S. and Chapman, T. M. US Patent No. Re34,123, November 10, 1992.
7. Kreiser, D. W., Dinkel, A. L., and Weibel, J. P. US Patent No. 6,197,840, March 6, 2001.
8. Wong, B., Zhang, Z., and Handa, Y. P. *J. Polym. Sci.: Part B: Polym. Phys.* 1998, **36**, 2025.
9. Handa, Y. P., Wong, B., Zhang, Z., Kumar, V., Eddy, S., and Kishan, K. *Polym. Eng. Sci.* 1999, **39**, 55.