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A New Technique for Measuring Retrograde Vitrification in Polymer–Gas Systems and for Making Ultramicrocellular Foams from the Retrograde Phase

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ABSTRACT: A stepwise temperature- and pressure-scanning thermal analysis method was developed to measure glass-transition temperature $T_g$ in the two-phase polymer–gas systems as a function of gas pressure $p$, and was used to confirm recent theoretical predictions that certain polymer–gas systems exhibit retrograde vitrification, that is, they undergo rubber-to-glass transition on heating. A complete $T_g$-$p$ profile delineating the glass–rubber phase envelope was established for the PMMA-CO$_2$ system. The retrograde vitrification behavior observed, where at certain gas pressures the polymer exists in the rubbery state at low and high temperatures and in the glassy state at intermediate temperatures, was similar to that reported previously based on the creep-compliance measurements. The existence of the rubbery state at low temperatures was used to generate foams by saturating the polymer with CO$_2$ at 34 atm and at temperatures in the range $-0.2$ to $24 \degree C$ followed by foaming at temperatures in the range $24$ to $90 \degree C$. Foams with very fine cell structure never reported before could be prepared by this technique. For example, PMMA foams with average cell size of $0.35 \mu m$ and cell density of $4.4 \times 10^{13}$ cells/g were prepared by processing the low temperature rubbery phase. © 2000 John Wiley & Sons, Inc. J Polym Sci B: Polym Phys 38: 716–725, 2000

Keywords: polymer; plasticization; gas; foams

INTRODUCTION

Compressed gases near or slightly above their critical points can dissolve to considerable extents in a glassy polymer causing a significant depression in the glass-transition temperature, $T_g$, of the polymer. This plasticization effect plays an important role in various areas including polymer membranes for gas separation; extraction of unreacted species or impurities from polymers; incorporation of additives into polymers; enhancing polymer–polymer miscibility; and facilitating making polymer blends or composites, polymer morphology modification, and fabrication of cellular polymers or polymer foams. For these applications, it is important to know the relationship between the polymer’s $T_g$ and the gas pressure, $p$, that is, the $T_g$-$p$ profile. For example, in developing processes for making polymer foams, a knowledge of the $T_g$-$p$ profile provides information on the conditions under which cell nucleation takes place, how the cellular morphology can be arrested, and the rheology of the polymer–gas system.

Over a limited pressure range, the $T_g$ of a polymer–gas system usually changes linearly with the gas pressure, as revealed by the results for a number of systems including polystyrene-CO$_2$, PS-ethylene, PS-HFC134a, polycarbonate-
CO\textsubscript{2},\textsuperscript{13,14} PVC-CO\textsubscript{2},\textsuperscript{13} PET-CO\textsubscript{2},\textsuperscript{15} and PMMA-CO\textsubscript{2},\textsuperscript{14,16} However, for the latter system, it was reported\textsuperscript{17} that at a CO\textsubscript{2} pressure of 39 atm, the system exhibited two \( T_g \)'s—a lower \( T_{g,l} \) at a temperature of 32.7 °C and a higher \( T_{g,h} \) at a temperature of 58.8 °C. This observation was later on accounted for by the theoretical models,\textsuperscript{18,19} which predicted that at a constant gas pressure or solubility, the polymer existed in the liquid (i.e., rubbery) state at temperatures below \( T_{g,l} \) and above \( T_{g,h} \), and in the glassy state at temperatures in between \( T_{g,l} \) and \( T_{g,h} \). The existence of \( T_{g,l} \) is attributed to enhanced solubility of the gas at lower temperatures. This unusual behavior was termed retrograde vitrification\textsuperscript{18} because, on heating under certain pressures, the polymer–gas system first exhibits a liquid-to-glass transition and then a glass-to-liquid transition. All the retrograde data reported in the literature on PMMA-CO\textsubscript{2} system were obtained by creep compliance measurements.\textsuperscript{17,20} In addition to PMMA-CO\textsubscript{2}, similar vitrification behavior was also found in the poly(ethyl methacrylate)-CO\textsubscript{2} system, again by creep compliance measurements.\textsuperscript{21}

A number of techniques have been used to measure \( T_g \) in polymer–gas systems.\textsuperscript{12,13} Of these, creep compliance is the only technique successfully used to establish the retrograde behavior. We tried the other \textit{in situ} techniques of high-pressure calorimetry\textsuperscript{12,16} and high-pressure DSC\textsuperscript{8,13,16} to measure the retrograde profile, but failed. The major reason that the temperature-scanning techniques are not well suited for such measurements is that it is not possible to keep the polymer–gas system in thermodynamic equilibrium during the heating or cooling runs. The glass transition is characterized by a constant pressure heat capacity \( C_p \) step-change. The precision in heat capacities determined using a DSC is often quite poor but can be improved considerably by using the stepwise heating or the enthalpy increment method.\textsuperscript{22} We have extended the stepwise \( C_p \) technique to the two-phase polymer–gas system to establish the \( C_p \) step and, thereby, determine the \( T_g \) of the system. Furthermore, the stepwise technique ensures that the thermodynamic equilibrium between polymer and gas is maintained throughout the measurements. In this article, we describe the stepwise \( C_p \) technique and show how it can be used to establish the \( T_g \)-\( p \) profile accurately and more efficiently than the creep compliance technique.

Cellular polymers with closed cells about 10 μm in size and a cell density of 10\textsuperscript{8} cells/cm\textsuperscript{3} are called microcellular foams\textsuperscript{23} and those with cells less than 1 μm in size and cell density greater than 10\textsuperscript{12} cells/cm\textsuperscript{3} are called ultramicrocellular (sometimes also called supermicrocellular) foams.\textsuperscript{24} These cellular polymers are made by saturating the polymer with a compressed gas and then subjecting the system to thermodynamic instability by either rapidly increasing the temperature or decreasing the pressure, causing the dissolved gas to escape. Provided that the polymer is above its plasticized \( T_g \) under such a treatment, the escaping gas leaves behind a cellular structure whose characteristics, cell size, and cell density depend on the temperature and pressure conditions under which the polymer was treated with the gas. In the various foaming methods reported in the open and patent literature, the processing of the polymer by the temperature increase or pressure drop is done above \( T_{g,h} \). In terms of the retrograde behavior, the polymer below \( T_{g,l} \) is in the same state as that above \( T_{g,h} \), and so, it should be possible to produce micro- or ultramicrocellular foams below \( T_{g,h} \). There are some other considerations that make foaming below \( T_{g,l} \) attractive: at low temperatures, the gas solubility may be quite high at relatively low pressures and the high dissolved-gas content may give a high cell density; the low temperature may facilitate better control on cell growth and may lead to much finer cells; and processing at low pressures can circumvent the safety and equipment cost concerns. In this article, we report on foaming PMMA below \( T_{g,l} \) using CO\textsubscript{2} as the blowing agent.

**EXPERIMENTAL**

PMMA from Canus Plastics was analyzed using GPC (Waters SEC equipped with a 401 DRI); it had \( M_w = 108,500 \) and \( M_n = 56,700 \). PMMA films around 300-μm thick and sheets around 1.25 mm were obtained by compression molding at 180 °C and then air quenched. High purity, bone dry CO\textsubscript{2} was used.

Setaram DSC121 was used for stepwise heat capacity measurements. Its temperature and energy scales were calibrated by measuring the heat capacities (in the stepwise mode, described below) of sapphire over the range of −40 to 140 °C, and by measuring, in the scanning mode, the melting points and heats of melting of high purity gallium, indium, tin, and zinc. The calibrations were...
then tested by conducting stepwise heat capacity measurements on benzoic acid (SRM 39i from NIST). The technique for making high-pressure measurements with the DSC121 has been described elsewhere. After installing the polymer film sample, the system was evacuated for a few hours to degas the polymer, and then both the reference and the measurement cells were pressurized to the desired pressure, $p$, monitored by a Setra pressure transducer (Model 204). The sample was held at a desired temperature in the range of $-10$ to $20 \, ^\circ C$ and sufficient time allowed for the polymer to attain equilibrium gas solubility.

Heat capacity measurements on the polymer–gas system were then made in the stepwise temperature or pressure-scanning mode. In the stepwise temperature scanning technique, the sample was held isothermally for 15 min to establish a baseline at the initial temperature $T_i$, then scanned at a rate of $1 \, ^\circ C/min$ to give a temperature jump of from 1 to 4 °C, and then held isothermally again for 15 min to establish a baseline at the final temperature $T_f$. These stepwise temperature jumps were continued until the desired temperature range was covered. The entire procedure was repeated with both reference and measurement cells containing the gas only at the same pressure as in the run with the polymer–gas system. Typical examples of the stepwise scans in the temperature range 0–12 °C are shown in Figure 1 for the sample (PMMA + CO$_2$) at 34 atm and the blank run with CO$_2$ at the same pressure. Also shown in Figure 1 are the corrected steps obtained by subtracting the blank run from the sample run. Integration of the peak for a given step yields the enthalpy increment $\Delta H$ required to affect the corresponding temperature change, $T_f-T_i$, and these two quantities then give, at the temperature $(T_f + T_i)/2$, the heat capacity $C_p$ of the polymer containing dissolved gas. It should be noted that, in our setup, the gas phase volume was much larger than the volume of the DSC cells such that during the temperature scan the pressure in the system remained constant. The $C_p$ of the polymer–gas system was obtained from the $C_p-T$ data (see below), and the entire procedure was repeated at several gas pressures in order to establish the $T_g-p$ profile.

In the stepwise pressure-scanning technique, the polymer was equilibrated with the gas at a pressure $p$ and a temperature jump made from $T_i$ to $T_f$. The system was then cooled back to $T_i$, the pressure was increased to the next value, and the temperature jump from $T_i$ to $T_f$ was made again once the polymer had equilibrated again with the new pressure. The system was cooled back to $T_i$, and the temperature jumps, from $T_i$ to $T_f$ continued at increasing pressures to obtain the $C_p-p$ curve, which then gave the plasticization pressure $p_g$ at $(T_f + T_i)/2$. The precision in $T_g$, measured by stepwise temperature or pressure jump, was $\pm 1 \, ^\circ C$.

For comparison, $T_g$ measurements were also made by equilibrating the polymer sample with the gas at a given pressure and temperature and then scanning the system at 5 °C/min. The details of the temperature scanning technique to establish the $T_g-p$ profile are given elsewhere. For solubility measurement at a given temperature and pressure, a known mass of the 1.25-mm thick PMMA sheet was first degassed for a few hours and then contacted with CO$_2$ in a pressure vessel made up of VCR fittings. The sample was taken out periodically and weighed to $\pm 0.1 \, mg$ until a constant mass was obtained. The total time taken for releasing the pressure, taking the sample out, and for weighing was within 1 min. Below the critical temperature of CO$_2$, solubility measurements were made by contacting the polymer with CO$_2$ in the compressed vapor or liquid state. The agreement between the solubility results obtained by dissolving CO$_2$ from the vapor or liquid phase was within $\pm 1.5\%$. Glassy polymers usually undergo irreversible dilation on exposure to high pressure CO$_2$. As a result, a
fresh sample was used for each pressure investigated.

For foaming, the polymer sheets were conditioned with compressed vapor or liquid CO$_2$ in the pressure vessel at the given temperature and pressure for 24 h, a time long enough to ensure establishment of the polymer–gas equilibrium. The pressure was then quickly released and samples brought to ambient conditions or transferred to a water bath held at various temperatures for foaming, followed by rapid quenching in ice-water slurry. The foaming time in water bath was 2 min, and the foams thus obtained were kept for at least 10 days prior to further analysis. The foam densities were measured by weighing the samples in air and in water. For microstructural analysis, a scanning electron microscope SEM (JEOL, JSM-5300) was used to take pictures of freshly exposed surfaces of foam samples fractured at liquid nitrogen temperature and then sputter coated with a thin layer of gold. The cells in the microphotographs were outlined manually and then rescanned into the computer for image analysis using the Image Pro Plus software from Media Cybernetics. For image analysis, the background of each scanned photograph was adjusted so that only the colored cells were visible on the monitor. All cellular characteristics such as equivalent diameter, perimeter, and area, and their distributions in each sample were obtained from the analysis, and the average cell size and cell density for a given foam sample were determined as described before.$^{10}$

Results and Discussion

Measurement of the Retrograde Profile

Heat capacities of neat PMMA at various temperatures measured by the stepwise technique are shown in Figure 2, and compared with data from the literature.$^{26}$ The agreement between the two sets of results is quite satisfactory, especially in the pre- and post-glass transition regions. A step increase in heat capacity with onset temperature of 95 °C and midstep temperature of 101 °C is clearly seen in our results. In this work, we will take the onset temperature as the $T_g$, though, in thermal analysis, it is customary to take the midpoint of the step transition as the $T_g$. We prefer to use the onset because it is established much more unambiguously, as shown in Figure 2, than the midpoint. Also shown in Figure 2 is a heating scan at 5 °C/min on neat PMMA. The $T_g$, again taken as the onset temperature, obtained from the scan is about 6 °C higher than that obtained from the $C_p$ measurements. This is reasonable because the stepwise heating allows the polymer segments much longer time to relax than the scanning method. A slightly higher $T_g$ is also seen in the literature $C_p$ values shown in Figure 2 as these were also obtained by scanning the sample.

The heat capacity of PMMA-CO$_2$ under a constant pressure of 34 atm is shown in Figure 3 as a function of temperature. It increases rapidly at temperatures above 50 °C, and goes through a step change similar to that shown in Figure 2. However, this time, the step occurs at a somewhat reduced temperature due to plasticization of PMMA by CO$_2$, and we identify the transition temperature as $T_{g,h}$. It should be noted that, for the stepwise heating, the holding time at each step (15 min) is comparable with the diffusive time scale of CO$_2$ in 300-μm thick PMMA and the step-to-step temperature jumps are quite small (1–4 °C). Therefore, the polymer–gas system can be considered to maintain equilibrium during the measurements with the dissolved gas content of the polymer decreasing slightly with each temperature jump. The $T_g$ obtained by the stepwise method thus corresponds to the true gas solubility at the transition temperature. On the other hand, in a scanning run, the temperature changes much faster than the gas diffusive time scale, and the
polymer–gas system is not really in equilibrium. As a result, the plasticized \( T_g \) measured by the scanning technique refers to a solubility at a somewhat lower temperature than the glass-transition temperature.

Surprisingly, at low temperatures, the heat capacity of the PMMA-CO\(_2\) system at 34 atm was found to decrease sharply with increasing temperature. The results are shown in Figure 4. This phenomenon was not observed in other polymer–gas systems, such as PS-CO\(_2\) and PS-ethylene, PVC-CO\(_2\), and PETG-CO\(_2\), in which the retrograde vitrification phenomenon has either not been reported or established firmly. Measurements at lower temperatures proved to be quite difficult due to proximity to the condensation conditions of CO\(_2\). The results shown in Figure 4 are for the conditions under which no condensed phase of CO\(_2\) was present in the system. As seen in Figure 4, the heat capacity of the system is unusually high, attaining a value of over 4.5 J K\(^{-1}\) g\(^{-1}\) at 1.3 °C. The results were quite reproducible, thereby, ruling out the presence of any condensed phase of CO\(_2\). Although the sorption of a small molecules results in an increase in polymer’s heat capacity as reported in the literature,\(^{27}\) and as is evident from Figures 2 and 3, the \( C_p \) increase in PMMA-CO\(_2\) solution at low temperatures is far beyond the anticipated effect. In view of the retrograde vitrification phenomenon reported in the literature,\(^{18}\) we assign the observed \( C_p \) behavior to the rubber-to-glass transition and identify the \( T_{g,l} \) as shown in Figure 4. Such a low-temperature transition, though easily measured by the stepwise method, cannot be detected by the conventional scanning method. This is because, for a given pressure, the difference between the \( T_{g,l} \) and the CO\(_2\) condensation temperature is too small to establish a stable baseline in a conventional DSC scan. It should be noted that the \( C_p \) change associated with the rubber-to-glass transition shown in Figure 4 is much larger than the corresponding change for the glass-to-rubber transition shown in Figure 3. At low temperatures, the system is very close to the saturation vapor pressure curve of CO\(_2\), and the dissolved CO\(_2\) is in a more liquidlike state.\(^{28}\) Consequently, it makes a much larger contribution to the \( C_p \) of the system than it would under conditions corresponding to the supercritical state of CO\(_2\), which is the case for the results shown in Figure 3.

Thus, by establishing the glass-to-rubber transition temperatures as illustrated in Figure 3 and the rubber-to-glass transition temperatures as illustrated in Figure 4, a complete \( T_g-p \) profile for PMMA-CO\(_2\) was generated, and is shown in Figure 5. The \( T_{g,l} \) and \( T_{g,h} \) curves meet at 43 °C and 58 atm. Also shown in Figure 5 is the saturation vapor pressure curve of CO\(_2\), which runs very close to the \( T_{g,l} \) curve. As mentioned above, DSC measurements were also made in the stepwise pressure-scanning mode. A set of typical results is shown in Figure 6 where the heat capacities of the PMMA-CO\(_2\) solution at 26 °C are plotted against the gas pressure. The onset of the transition gives a plasticization pressure \( p_g \) of 47 atm. This is in good agreement with a \( T_g \) of 26 °C at 49 atm

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**Figure 3.** \( C_p \) of PMMA-CO\(_2\) solution as a function of temperature under a CO\(_2\) pressure of 34 atm. A solid curve is drawn through the \( C_p \) results to elaborate the glass transition.

**Figure 4.** \( C_p \) of PMMA-CO\(_2\) solution at low temperatures and a CO\(_2\) pressure of 34 atm. A solid curve is drawn through the \( C_p \) results to elaborate the glass transition. \( \bullet \), first run; \( \square \), second run.
Thus, even though the two techniques give similar results, the stepwise temperature scanning method is the preferred technique as it is about 30 times faster than the stepwise pressure-scanning method. The result in Figure 5 shows the so-called retrograde vitrification behavior previously reported for this system. For example, consider the PMMA-CO$_2$ system at 40 atm and 2 °C. Then, according to Figure 5, these $T$, $p$ conditions define a state in-between the CO$_2$ saturation vapor pressure curve and the $T_{g,l}$ curve. The system under these conditions is in the rubbery state. On heating at 40 atm, the system enters the phase envelope where it exists as a glass. Thus, a rubber transforms to glass on heating or, if the isobaric process is reversed, the glass transforms to rubber on cooling, and this is termed the retrograde vitrification. Another feature of note is that over a certain pressure range, there exist two $T_{g}$'s at a given pressure. Accordingly, on heating at 40 atm, the system will first undergo a rubber-to-glass transition at about 14.4 °C and then a glass-to-rubber transition at about 67.8 °C.

The retrograde vitrification profile measured here is similar to that reported in the literature based on creep compliance measurements. The literature results are shown in Figure 5. The agreement between the two sets of results is quite good considering the difference in the measurement techniques and in the assignment of the transition temperature. As seen in Figure 5, the window between the glass-transition line, $T_{g,l}$, and the CO$_2$ condensation line is quite small. This excludes the application of conventional scanning methods in measuring $T_{g}$ in such polymer–gas systems. Accordingly, the isobaric stepwise temperature scanning technique, the pseudoisothermal stepwise pressure-scanning technique, and the isothermal pressure-scanning technique (creep compliance) are deemed useful for characterizing the retrograde behavior. It is easier to automate the programmed temperature ramping than pressure ramping, and the small thermal mass associated with the DSC vessels allows temperature equilibrium to be established rapidly. In this context, the isobaric stepwise heating method developed here is more efficient and easier to use than the other techniques. It should, however, be noted that the measurements terminate at the point where the $T_{g,l}$ curve intersects the CO$_2$ condensation curve. Both methods, stepwise thermal analysis and pressure-scanning creep compliance measurements, share this limitation.

Retrograde vitrification is conjectured to occur because of the rather high gas solubility of CO$_2$ at low temperatures, especially at temperatures below the critical temperature of CO$_2$. In order to confirm this, the solubility $S$ of CO$_2$ in PMMA was measured under a constant pressure of 34 atm and at various temperatures. Figure 7 shows the van’t Hoff plot of the solubility in the temperature range $-0.2$–$110$ °C. A rapid increase in solubility is seen at temperatures below about 9.5 °C. This exceptionally high solubility under conditions...
where the system approaches the saturation vapor pressure curve of CO$_2$ was also predicted theoretically.$^{18,19}$ This enhanced solubility is, in fact, responsible for the existence of the rubbery state at low temperatures as shown in Figure 5, or conversely, the rapid decrease in solubility on heating the low temperature phase is responsible for the rubber-to-glass transition identified as $T_{g,l}$ in Figure 4. The existence of the rubbery state at low temperatures is further supported by the sorption kinetics results shown in Figure 8; gas sorption occurs more rapidly at $-0.2 \, ^{\circ}C$ than at $24 \, ^{\circ}C$ because of the much faster diffusion of CO$_2$ at the lower temperature. A detailed investigation on the solubility and diffusivity of CO$_2$ in PMMA over extended ranges of temperature and pressure is now in progress in our laboratory.

The Effect of Retrograde Vitrification on Foaming

A polymer containing dissolved gas can be foamed by rapidly releasing the gas pressure (called pressure quench method) or by rapidly heating the polymer–gas solution (called the temperature soak method). In either method, the polymer–gas system should be above its plasticized $T_g$ for the foaming to occur. Thus, the $T_g$-$p$ profile identifies the necessary conditions for foaming. For systems exhibiting retrograde behavior, such as that shown in Figure 5, the pressure quench method will apply when the polymer is saturated with the gas or liquid within the retrograde envelope—the glassy region. This has been proven by our experiments under various conditions. In our work, no foams were obtained when the polymer was saturated within the glassy region and then subjected either to pressure quench or heated to within $5 \, ^{\circ}C$ of the phase boundary after the pressure was released, whereas a variety of foams could easily be produced from the rubbery phases that exist above $T_{g,h}$ or below $T_{g,l}$.

Other factors, such as the activity of CO$_2$ and the polymer viscosity, also determine whether cell nucleation and growth will occur or not. For example, at $-0.2 \, ^{\circ}C$ and 34 atm, although PMMA is in the rubbery state and the gas solubility is quite high, no foaming was observed on pressure quench. This is attributed to the rather poor performance of CO$_2$ as a blowing agent under conditions close to its saturation vapor pressure curve. However, at slightly elevated temperatures and pressures, $24 \, ^{\circ}C$ and 53 atm, PMMA could be easily foamed by simply releasing the gas pressure, and foaming by the pressure quench method occurred most efficiently at pressures above the maximum retrograde pressure $p_{g,\text{max}}$ of 58 atm, or at temperatures above $T_{g,h}$. These observations suggest that high viscosity of the macromolecules and the reduced activity of CO$_2$ at low temperatures prevent foaming by the pressure quench method. They also suggest that slight heating of the samples saturated under conditions corresponding to the lower end of the $T_{g,l}$ curve should favor foaming. This indeed was found to be the

Figure 7. Solubility of CO$_2$ at 34 atm in PMMA plotted against reciprocal temperature. The solid line represents the van't Hoff fit to the data in the temperature range of about 10 to 110 °C.

Figure 8. A comparison of the sorption kinetics of 34 atm CO$_2$ in PMMA at $-0.2 \, ^{\circ}C$ and $24 \, ^{\circ}C$. Solid curves are drawn through the data points to elaborate the markedly different sorption rates.
case. For example, the PMMA sample saturated at \(-0.2\) °C and 34 atm easily foamed when heated to a temperature above 10 °C. As shown in Figure 9, foams with fine closed-cell structure were obtained when such a sample was quickly heated to a temperature in the range 24 to 80 °C.

The retrograde behavior also affects the morphology of the foamed polymer. Foams with cell size less than 5 μm, such as those shown in Figure 9, were obtained only if the polymer was saturated at conditions below the \(T_{g,l}\) curve or at temperatures below \(T_{g,h}\) and at pressures beyond \(P_{g,\text{max}}\). On the other hand, if the polymer was saturated with CO\(_2\) at 24 °C and 34 atm, that is, inside the retrograde envelope, and then heated to 80 °C—a temperature just above the \(T_{g,h}\) at 34 atm—closed-cell foams with much larger cells (about 40 μm) were obtained, the cell size being about 100 times that shown in Figure 9. It should be noted that PMMA foams with cellular characteristics comparable to those shown in Figure 9 have previously been produced at temperatures in the range 30 to 60 °C and at pressures over 130 atm. The latter pressure is much higher (values of 30–50 atm) than the pressures required for producing foams from the retrograde phase.

The effect of saturation conditions on foam morphology can be attributed to the variation of CO\(_2\) solubility with temperature. Figure 10

Figure 10. Cell density and average cell size of PMMA foams as a function of CO\(_2\) solubility in the polymer. All samples were foamed at 80 °C. A solid curve is drawn through the data points to show the trend.

Figure 11. Cell density and average cell size of PMMA foams as a function of foaming temperature. Foam samples were obtained from PMMA saturated with 34 atm CO\(_2\) at \(-0.2\) °C. A solid curve is drawn through the data points to show the trend.
shows the dependence of cell density and cell size on CO$_2$ solubility for the PMMA samples foamed at 80 °C. It is clear that solubility plays a vital role in controlling cell density and cell size. The equilibrium solubility of CO$_2$ in PMMA is 22.5 wt % at $0.2 \, ^\circ\text{C}$ and 34 atm and decreases rapidly to 7.9 wt % at 24 °C and 34 atm. This gives rise to quite different foam morphologies as reported above. Since exceptionally high gas solubilities can be achieved at conditions below the $T_g,l$ curve, micro- and ultramicrocellular foams with unique morphologies can be generated. Figures 11 and 12 show, respectively, the cell density, cell size, and foam density of microcellular PMMA as a function of foaming temperature after the polymer was saturated with CO$_2$ at $0.2 \, ^\circ\text{C}$ and 34 atm. With increasing temperature, cell nucleation rate increases, resulting in an increase in cell density and reduction in cell size and foam density. The nucleation effect, however, levels off at high temperatures because of cell coalescence. Thus, by optimizing the foaming temperature, PMMA foam with an average cell size of 0.35 $\mu$m, cell density of $4.4 \times 10^{13}$ cells/g, and foam density of 0.116 g/cm$^3$ can be made after saturating the polymer with CO$_2$ at $-0.2 \, ^\circ\text{C}$ and 34 atm. The production of such an ultramicrocellular structure at low pressures has not been reported in the literature. For example, a minimum cell size of 0.5 $\mu$m and a maximum cell density of $10^{12}$ cells/cm$^3$ has been reported when PMMA was saturated with CO$_2$ at 40 °C and 272 atm.\textsuperscript{9,29}

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**REFERENCES AND NOTES**